

2006 JAWAHARLAL NEHRU TECHNOLOGICAL UNIVERSITY

IV B.TECH II SEMESTER SUPPLEMENTARY EXAMINATIONS
OPTIMIZATION OF CHEMICAL PROCESSES
 (CHEMICAL ENGINEERING)

APR/MAY 2006

TIME - 3 HOUR
 MARK - 80

Answer any FIVE Questions
All Questions carry equal marks

1. (a) Discuss the problem of optimization of economic insulation thickness. [6]
- (b) Assume that the bare surface of a vessel is at 7000F with an ambient temperature of 700F. The surface heat loss is 4000 Btu/(h) (ft²). Add one inch of calcium silicate insulation and the loss will drop to 250 Btu/(h)(ft²). At an installed cost of \$ 4/ (ft²) and a cost of energy at \$ 5/106 Btu, a saving of \$ 164 per year (8760 hours of operation) per square foot would be realized. Calculate the pay back period and mention the approach to determine the optimum insulation thickness. [10]
2. Formulate net present value for a project lasting n years with an initial investment I_0 , interest rate of capital i , constant annual expense E , constant annual revenue A , salvage value S_v , yearly depreciation D_j , and a tax rate t . Compare NPV for tax rates of 0 and 50 percent, $S_v = 0$, and straight-line depreciation. Use $n = 10$ and $i = 0.15$ ($r = 0.2$). [16]
3. Explain the difference between uni model and multi model functions [16]
4. Use the simplex procedure with un restricted variables minimize $f(x) = x_1 + 4x_2$ subject to $x_1 + x_2 \leq 3$ - $x_1 + x_2 \leq 1$ x_1 unrestricted, $x_2 \geq 0$ find the optimal values of x_1 and x_2 ? [16]
5. For a waste heat recovery system the following data are given: Cost per unit area of exchanger, $CA = Rs.20/ft^2$ Value of power, incorporating necessary conversion factors to have a consistent set of units, $CH = 1.76 \times 10^{-5}$ Average overall heat transfer coefficient, $U = 95 \text{ Btu/(h)(oF)(ft}^2)$ Number of hours per year of operation, $y = 8760 \text{ h/year}$ Annualization factor for capital investment, $r = 0.365$ Efficiency of overall system, $\eta = 0.7$ Condensing temperature, $T_2 = 600 \text{ oR}$ Average hot fluid temperature, $T_s = 790 \text{ oR}$ Calculate the optimum value of the working fluid temperature, TH .
6. Explain the procedure involved for determining the optimum reflux ratio for a staged distillation column applying the one dimensional search technique of optimization. [16]
7. The cost function C representing the annual costs of a pipe line transporting a fluid is given by $C = C_1 D^{1.3} L + 0.142 (C_0 / \eta) m^{2.8} \mu^{0.2} \rho^{-2.0} D^{-4.8} L$ where the cost coefficients are considered as $C_0 = Rs. 0.59$ and $C_1 = Rs. 5.7$. The mass flow rate of fluid $m = 25 \text{ kg/s}$, density $\rho = 1000 \text{ kg/m}^3$, $\mu = 1.08 \times 10^{-3} \text{ N/s m}^2$, the pumping efficiency $\eta = 0.60$ and the pipe length $L = 10 \text{ m}$. Find the optimal pipe diameter D_{opt} [16]
8. The steady state dependence of chemostat variables, namely, cell mass concentration x and substrate concentration s are expressed by the following equations: $x = yx/s hSf - DKs \mu_{max} - Di$ $s = DKs \mu_{max} - D$ where D is the dilution rate. The parameter values are: maximum specific growth rate $\mu_{max} = 1.0 \text{ h}^{-1}$, yield factor $Y_{x/s} = 0.5$, substrate growth rate constant $K_s = 0.2 \text{ g/lit}$ and substrate feed concentration $s_f = 10.0 \text{ g/lit}$. The rate of cell mass production per unit reactor volume is Dx . Show that the system exhibits washout condition at $D = \mu_{max}$ ical fertilizer plant? [16]